

Correction

Phase Equilibrium of Ethanol + CO₂ and Acetone + CO₂ at Elevated Pressures. Chany-Yih Day, Chieh-ming J. Chang, and Chiu-Yang Chen, *J. Chem. Eng. Data* **1996**, *41*, 839-843.

Tables 1 and 2 are incorrect. The correct tables are shown below.

Table 1. Experimental Data for Carbon Dioxide (1) + Ethanol (2)

<i>P</i> /MPa	<i>x</i> ₁	<i>y</i> ₁	ρ^V /kg·m ⁻³	ρ^L /kg·m ⁻³	<i>P</i> /MPa	<i>x</i> ₁	<i>y</i> ₁	ρ^V /kg·m ⁻³	ρ^L /kg·m ⁻³	<i>P</i> /MPa	<i>x</i> ₁	<i>y</i> ₁	ρ^V /kg·m ⁻³	ρ^L /kg·m ⁻³
<i>T</i> = 291.15 K														
1.16	0.1652	0.9835	12.5	801.7	2.41	0.3257	0.9907	46.5	821.6	3.45	0.4684	0.9919	74.1	834.1
1.57	0.1944	0.9852	19.9	806.5	2.81	0.3712	0.9918	56.6	825.1	3.84	0.5847	0.9905	86.4	836.6
1.86	0.2355	0.9874	30.2	811.6	3.10	0.4197	0.9927	64.1	829.4	4.36	0.7262	0.9895	105.2	844.2
2.14	0.2769	0.9887	39.6	817.2										
<i>T</i> = 298.17 K														
1.16	0.1305	0.9855	34.0	797.9	2.96	0.3273	0.9906	80.3	813.8	5.39	0.6866	0.9879	163.5	841.2
1.62	0.1865	0.9873	49.3	804.6	3.65	0.4103	0.9918	99.6	819.7	5.82	0.8139	0.9860	187.8	847.6
2.28	0.2624	0.9895	63.9	809.7	4.34	0.5172	0.9905	121.1	828.1					
<i>T</i> = 303.12 K														
1.16	0.0978	0.9845	12.2	787.8	3.89	0.3641	0.9910	81.7	810.1	5.93	0.6499	0.9885	159.5	828.4
1.64	0.1353	0.9858	27.5	792.4	4.25	0.4158	0.9917	92.9	813.9	6.27	0.7893	0.9843	179.7	832.9
2.43	0.2075	0.9880	44.0	796.5	4.95	0.4916	0.9913	116.8	817.0	6.48	0.8486	0.9829	193.8	836.7
2.91	0.2746	0.9896	55.4	807.2	5.58	0.5798	0.9903	142.6	821.2					
<i>T</i> = 308.11 K														
1.57	0.1159	0.9841	19.0	791.6	4.39	0.3325	0.9916	111.5	816.8	6.31	0.5822	0.9907	185.5	830.1
2.09	0.1591	0.9860	30.2	796.6	4.87	0.3808	0.9919	126.7	819.1	6.66	0.6367	0.9894	205.4	833.0
2.58	0.1957	0.9877	45.3	800.8	5.16	0.4018	0.9919	136.5	823.0	6.89	0.7247	0.9857	221.2	834.7
3.09	0.2239	0.9897	67.9	807.0	5.68	0.4589	0.9920	156.0	825.0	7.01	0.7721	0.9840	230.4	835.9
3.65	0.2594	0.9912	90.2	810.4	6.01	0.5290	0.9917	170.5	864.2	7.17	0.8258	0.9827	243.8	836.1
4.00	0.2904	0.9915	99.8	813.4										
<i>T</i> = 313.14 K														
0.91	0.0529	0.9849	8.5	777.9	4.97	0.3200	0.9912	102.5	803.3	7.02	0.5399	0.9886	186.4	818.4
1.84	0.1009	0.9864	26.3	784.7	5.49	0.3609	0.9918	119.6	806.5	7.31	0.5844	0.9865	204.0	821.5
2.92	0.1718	0.9877	48.7	790.1	5.90	0.3999	0.9922	134.9	809.9	7.60	0.6593	0.9823	222.9	822.5
3.93	0.2280	0.9894	73.7	799.1	6.31	0.4398	0.9912	151.3	813.5	7.73	0.7492	0.9770	233.9	823.1
4.50	0.2800	0.9905	88.8	800.8	6.65	0.4897	0.9900	166.8	815.6	7.92	0.8210	0.9725	252.0	826.0

Table 2. Experimental Data for Carbon Dioxide (1) + Acetone (2)

<i>P</i> /MPa	<i>x</i> ₁	<i>y</i> ₁	ρ^V /kg·m ⁻³	ρ^L /kg·m ⁻³	<i>P</i> /MPa	<i>x</i> ₁	<i>y</i> ₁	ρ^V /kg·m ⁻³	ρ^L /kg·m ⁻³	<i>P</i> /MPa	<i>x</i> ₁	<i>y</i> ₁	ρ^V /kg·m ⁻³	ρ^L /kg·m ⁻³
<i>T</i> = 291.15 K														
0.87	0.2150	0.9745	11.6	806.8	2.81	0.5940	0.9881	55.6	829.4	4.34	0.8175	0.9842	104.3	848.3
1.18	0.2885	0.9794	17.9	812.5	3.10	0.6545	0.9904	63.7	826.1	4.94	0.8659	0.9806	131.3	851.1
1.73	0.4027	0.9827	29.6	819.2	3.45	0.7119	0.9885	73.7	840.9	5.27	0.9097	0.9785	150.2	853.3
2.41	0.5208	0.9848	45.5	824.4	3.84	0.7669	0.9868	86.1	844.6					
<i>T</i> = 298.16 K														
0.88	0.1699	0.9729	11.1	792.5	2.60	0.4687	0.9833	48.0	827.4	4.34	0.7472	0.9868	97.6	859.3
1.27	0.2460	0.9752	18.9	804.3	2.96	0.5290	0.9858	57.1	835.4	4.69	0.7921	0.9826	109.8	862.0
1.62	0.3125	0.9796	26.2	810.0	3.33	0.5888	0.9896	66.5	842.7	5.00	0.8379	0.9783	122.5	864.4
1.96	0.3701	0.9812	33.6	818.0	3.65	0.6406	0.9902	76.0	848.9	5.39	0.8922	0.9733	139.8	866.9
2.28	0.4190	0.9834	40.4	822.8	4.00	0.6950	0.9899	86.4	856.6	5.82	0.9345	0.9683	164.0	869.5
<i>T</i> = 303.13 K														
0.87	0.1655	0.9605	9.5	788.9	2.91	0.4823	0.9815	52.2	821.0	4.95	0.7735	0.9864	114.2	847.5
1.31	0.2360	0.9658	18.0	796.5	3.42	0.5698	0.9844	65.7	828.7	5.31	0.8162	0.9838	128.1	852.1
1.65	0.2927	0.9696	24.6	804.0	3.89	0.6239	0.9869	78.8	835.4	5.58	0.8496	0.9811	140.1	854.7
2.01	0.3482	0.9731	31.9	809.5	4.25	0.6882	0.9894	90.0	839.2	5.93	0.8864	0.9782	157.1	856.6
2.43	0.4191	0.9771	40.9	814.5	4.56	0.7311	0.9886	100.5	842.4	6.27	0.9189	0.9754	176.8	858.1
<i>T</i> = 308.15 K														
0.82	0.1620	0.9548	3.1	783.7	3.65	0.5474	0.9817	68.8	820.0	6.01	0.8296	0.9835	149.0	876.7
1.32	0.2250	0.9592	13.1	788.9	4.00	0.6001	0.9809	78.5	822.6	6.31	0.8609	0.9818	163.7	841.4
1.57	0.2650	0.9649	18.6	797.5	4.39	0.6508	0.9810	89.8	827.2	6.66	0.8896	0.9758	183.0	843.3
2.09	0.3350	0.9726	30.7	802.2	4.87	0.7014	0.9824	105.0	831.9	7.01	0.9257	0.9714	206.0	844.9
2.58	0.4078	0.9782	42.4	806.6	5.16	0.7481	0.9831	115.0	834.1	7.17	0.9366	0.9686	218.9	845.7
3.13	0.4787	0.9805	55.5	817.9	5.68	0.8003	0.9833	134.7	837.3					
<i>T</i> = 313.13 K														
0.78	0.1426	0.9339	6.7	774.8	2.80	0.4029	0.9653	46.4	802.7	5.17	0.6814	0.9885	109.3	825.8
1.18	0.1857	0.9421	13.9	785.0	3.24	0.4615	0.9714	56.5	807.7	5.48	0.7313	0.9855	119.8	827.5
1.57	0.2421	0.9496	21.2	789.5	3.61	0.5276	0.9773	65.4	812.4	5.91	0.7860	0.9814	135.7	829.1
2.03	0.3043	0.9562	30.4	793.7	4.06	0.5679	0.9830	76.9	816.9	6.44	0.8394	0.9785	157.6	830.0
2.47	0.3590	0.9599	39.4	798.7	4.60	0.6187	0.9857	92.0	821.7	7.39	0.9039	0.9754	208.8	828.7

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